

# 中国煤制烯烃技术进展

## Coal-to-Olefin Technology in China

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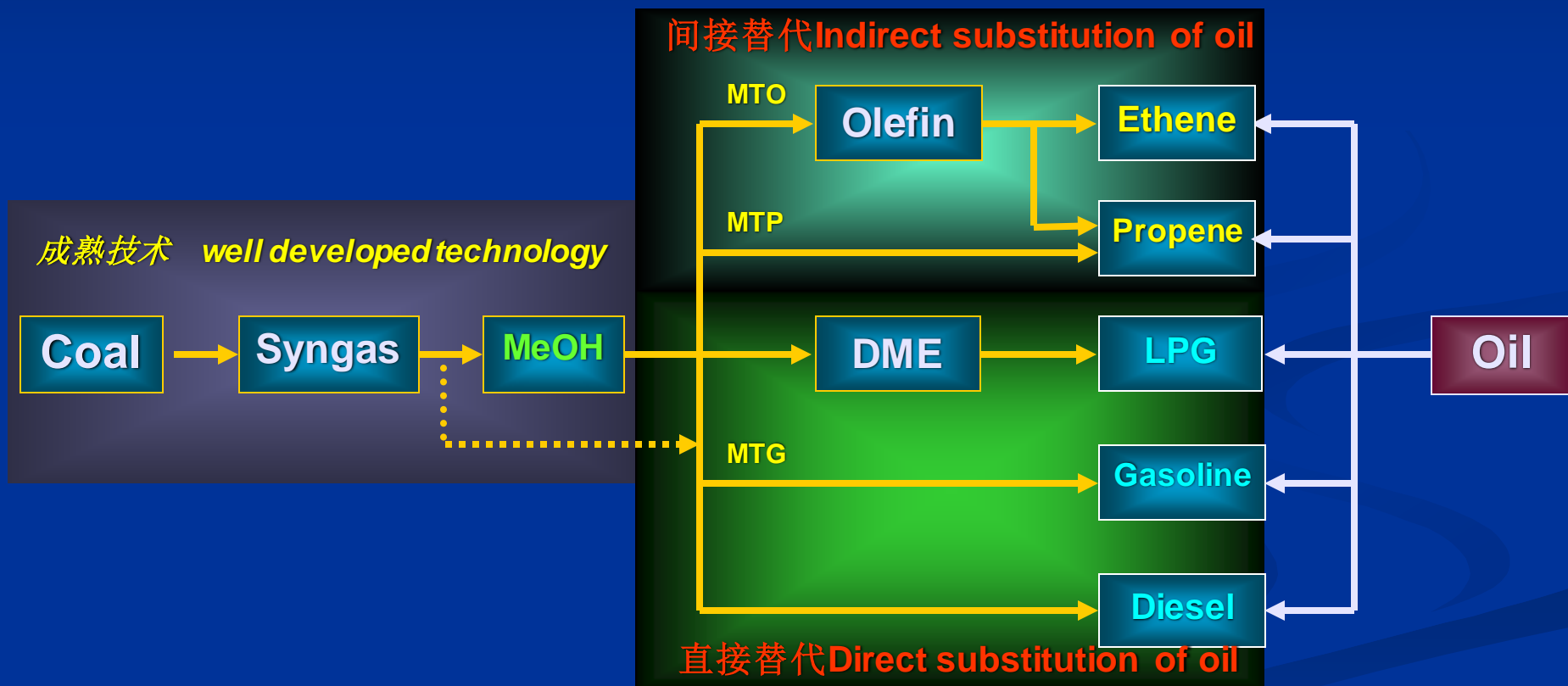
2009.12.03

# 内容 Content

- **背景 Background**
- **甲醇制乙烯和丙烯 Methanol to Ethylene and Propylene**
  - **DMTO技术 DMTO technology**
  - **技术经济 Economics**
  - **工业化 Commercialization**
- **甲醇制丙烯 Methanol to Propylene**
  - **FMTP技术 FMTP technology**

# 甲醇：联系煤化工与石油化工的桥梁

## Methanol: an important product linking petrochemicals to coal chemical industry



# 烯烃生产技术路线和MTO

## Technical Routes for Olefin Production & MTO

### Naphtha Feedstock

China	US	Japan
67%	39%	93%

石脑油  
Naphtha

$>800^{\circ}\text{C}$ ,  $\text{H}_2\text{O}$ ,  $\text{C}_2^+=\text{C}_3^+$   
Yield  $\sim 45\%$

乙烷  
Ethane

$>800^{\circ}\text{C}$ ,  $+\text{H}_2\text{O}$

煤、天然气  
Coal, Natural Gas

合成气  
Syngas

甲醇  
Methanol

DMTO  
(MTO)

乙烯

丙烯

$\text{C}_2\text{H}_4$

$\text{C}_3\text{H}_6$

Well developed technology



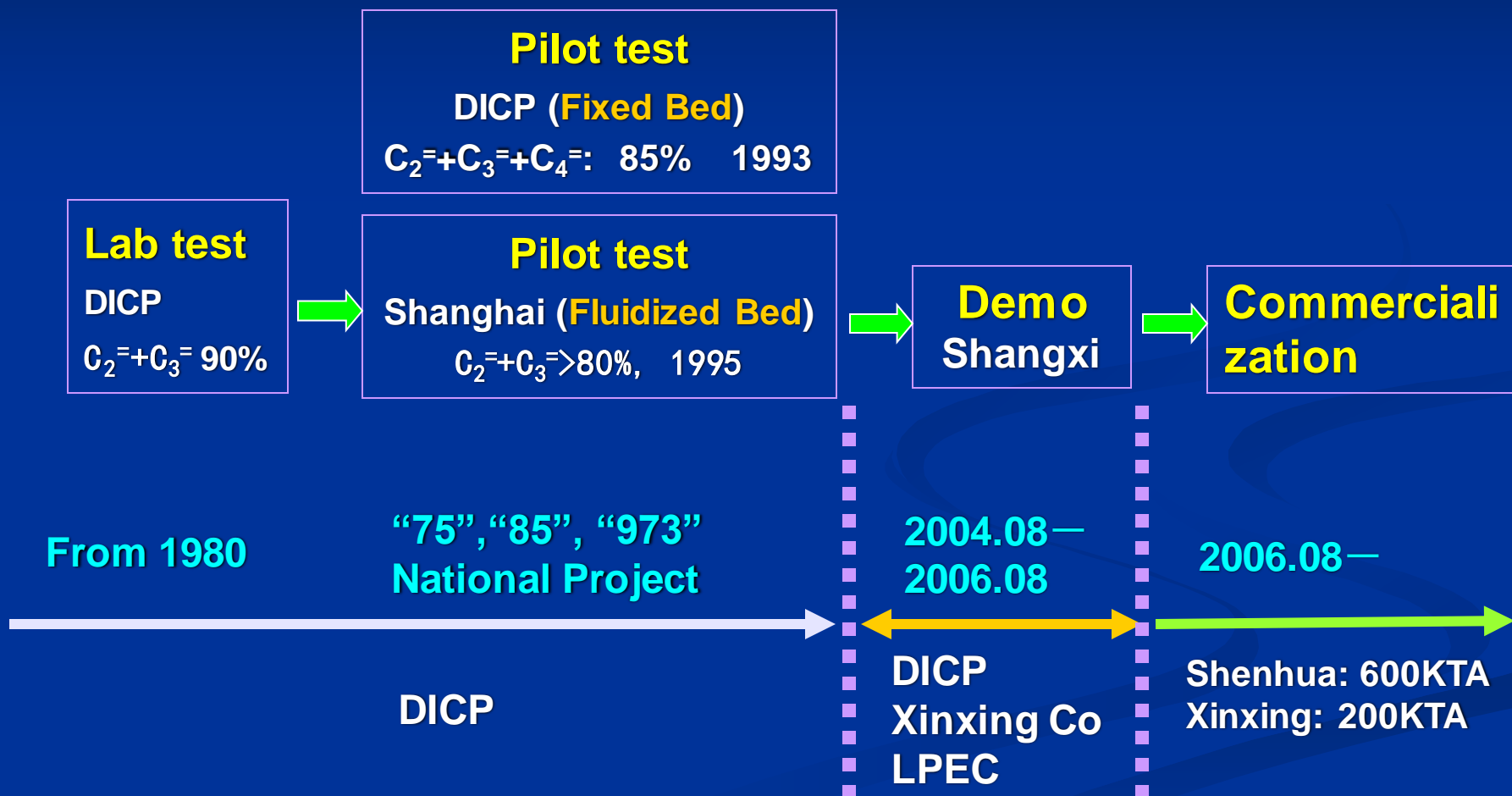
## MTO反应特点

# Characteristic of Methanol to Olefin reaction

- 酸性催化特征      Acid catalyzed reaction
- 高转化率：100%      High conversion
- 低压反应      Low pressure is favorable to light olefin selectivity
- 强放热      Exothermic reaction
  - 400-500°C, 100% conversion
  - $\Delta H = -22.4 \sim -22.1$  KJ/mol methanol
- 快速反应      Fast reaction
  - 100% conversion at 0.04s contact time
- 分子筛催化的形状选择性效应：高选择性      Shape selective effect  
should be applied for high olefin selectivity
  - First generation of catalyst: Modified ZSM-5
  - Small pore SAPO molecular sieve could be good candidate for developing new catalyst

# 大连化物所DMTO研究历程

## DMTO R&D in DICP



## DMTO技术

## SAPO分子筛的研究

# DMTO technology *Research on Small pore SAPO molecular sieves*

- 早期专利 UCC patent in 1982 (USP4440871) on SAPOs

- DICP首次报道了SAPO-34对MTO的优异性能

DICP first demonstrated good performance of SAPO-34 in MTO reaction

- *Applied Catalysis, Vol.40, No1-2, p316, 1988 ; Applied Catalysis, vol.64, p31-40, 1990*

- DICP对SAPO分子筛的合成及机理进行了系统深入的研究

Synthesis and mechanism were well studied on small pore SAPO molecular sieves

- 集中于SAPO-34

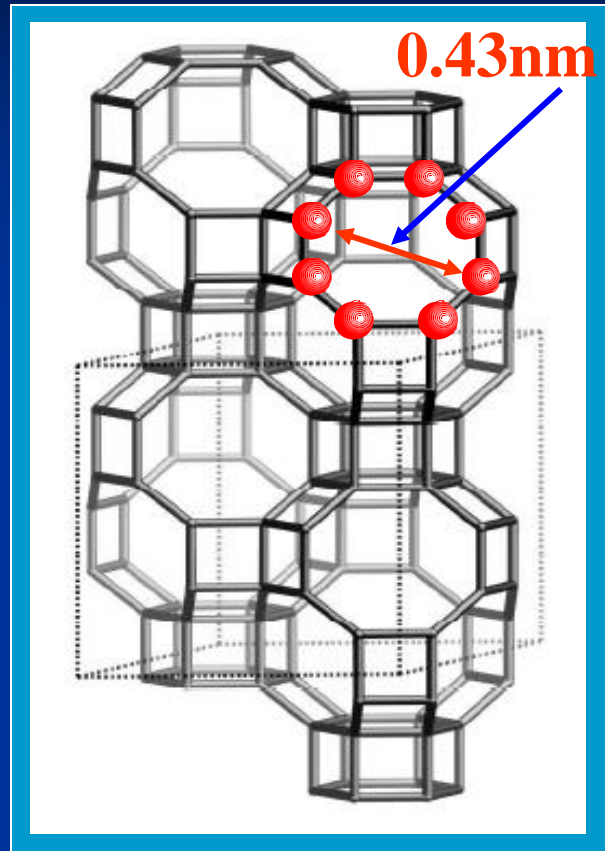
Focused on SAPO-34

- 其他小孔SAPO分子筛  
and tested

Other small pore SAPOs were also synthesized

# SAPO-34分子筛

## SAPO-34 Molecular Sieve

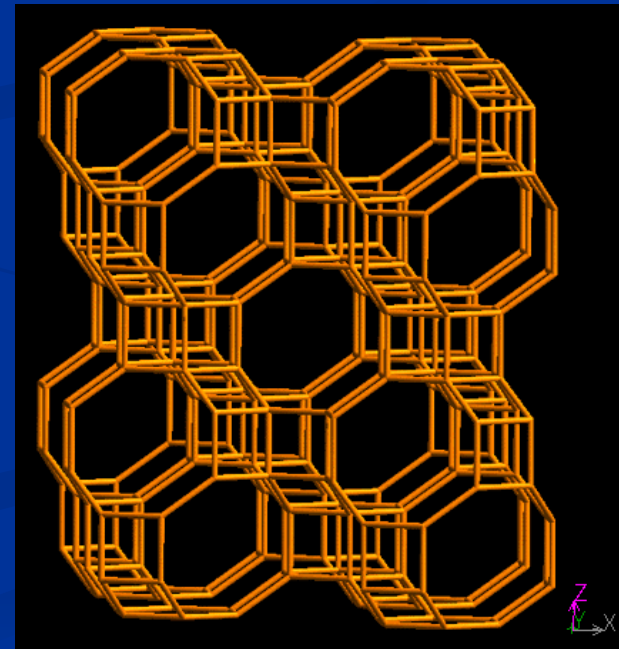


$C_2H_4$   
0.39nm

$C_3H_6$   
0.43nm

$C_6H_6$   
0.58nm

SAPO-34 framework  
CHA-type



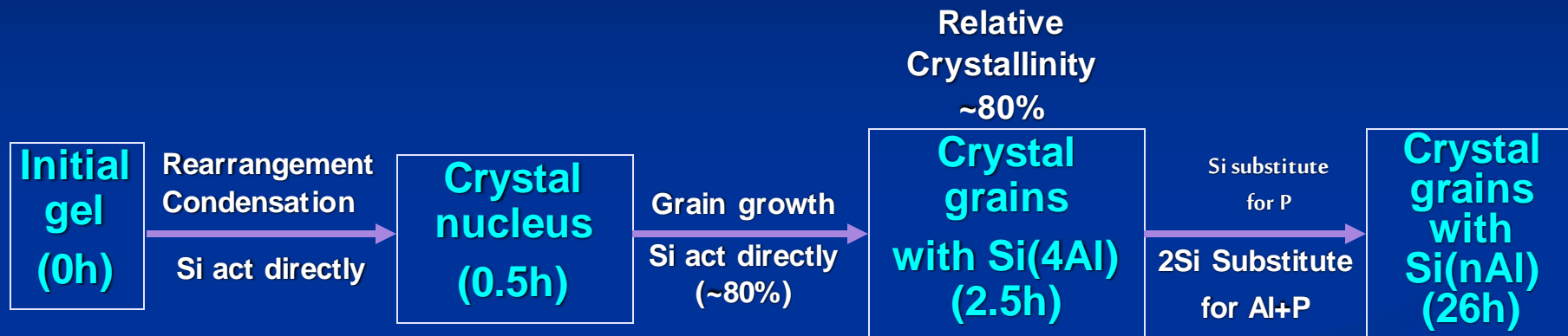
# SAPO-34合成方法的创新

## New methods for SAPO-34 synthesis

	Template 模板剂	
First patent	tetraethylammonium hydroxide	USA4440871
DICP	triethylamine (TEA), diethylamine (DEA), TEA+DEA	EP1142 833A1
Other Methods	dipropylamine, isopropylamine, piperidine, Morpholine	

# SAPO-34的晶化机理

## Crystallization mechanism of SAPO-34



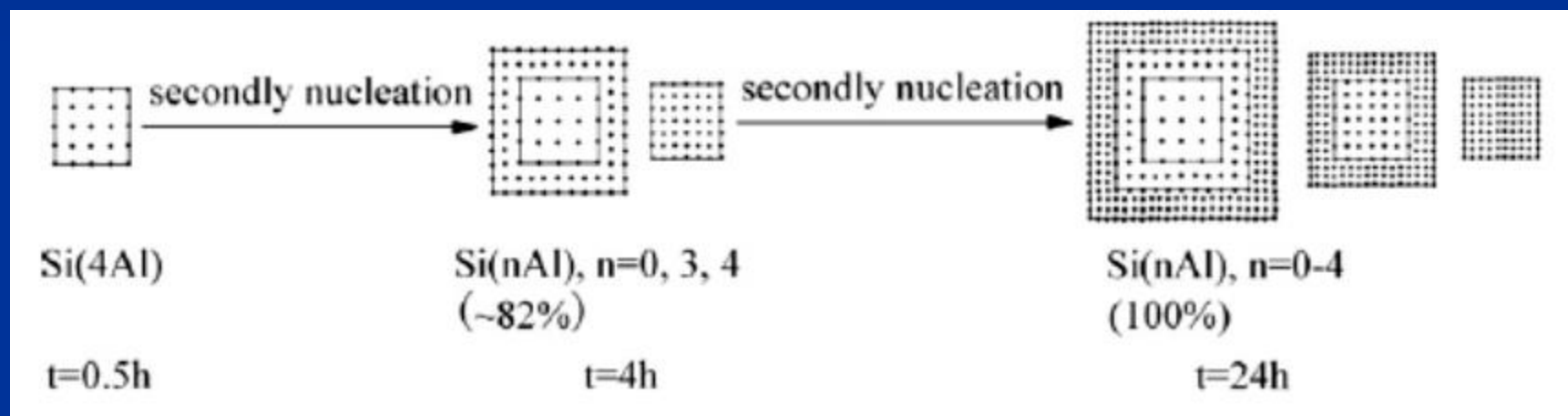
- *MICROPOROUS AND MESOPOROUS MATERIALS*, 115 (3): 332-337 NOV 1 2008, **Synthesis of SAPO-34 with only Si(4Al) species: effect of Si contents on Si incorporation mechanism and Si coordination environment of SAPO-34**
- **PCT/CN2007/002375**
- **PCT/CN2007/002376, PCT/CN2007/002332, PCT/CN2007/002333**

# SAPO-34的晶化机理

## Crystallization mechanism of SAPO-34

晶化过程中Si在晶粒中的非均匀分布模型

Schematic diagram of crystallization process with Si distribution in the crystals



*Microporous and Mesoporous Materials, 114 (1-3): 416-423 SEP 1 2008*

# Development of fluidized catalyst

喷雾干燥系统

Spring Dryer for  
Fluidized Catalyst  
Preparation



## 提升管反应系统

### Fluidized Reaction System

(raiser reactor, continuous  
reaction-regeneration)

Catalyst loading amount:

10kg



## 密相循环流化床反应系统

Dense Phase Fluidized  
Reaction System with  
Catalyst Recycling and  
product separation

Catalyst loading amount:  
20kg



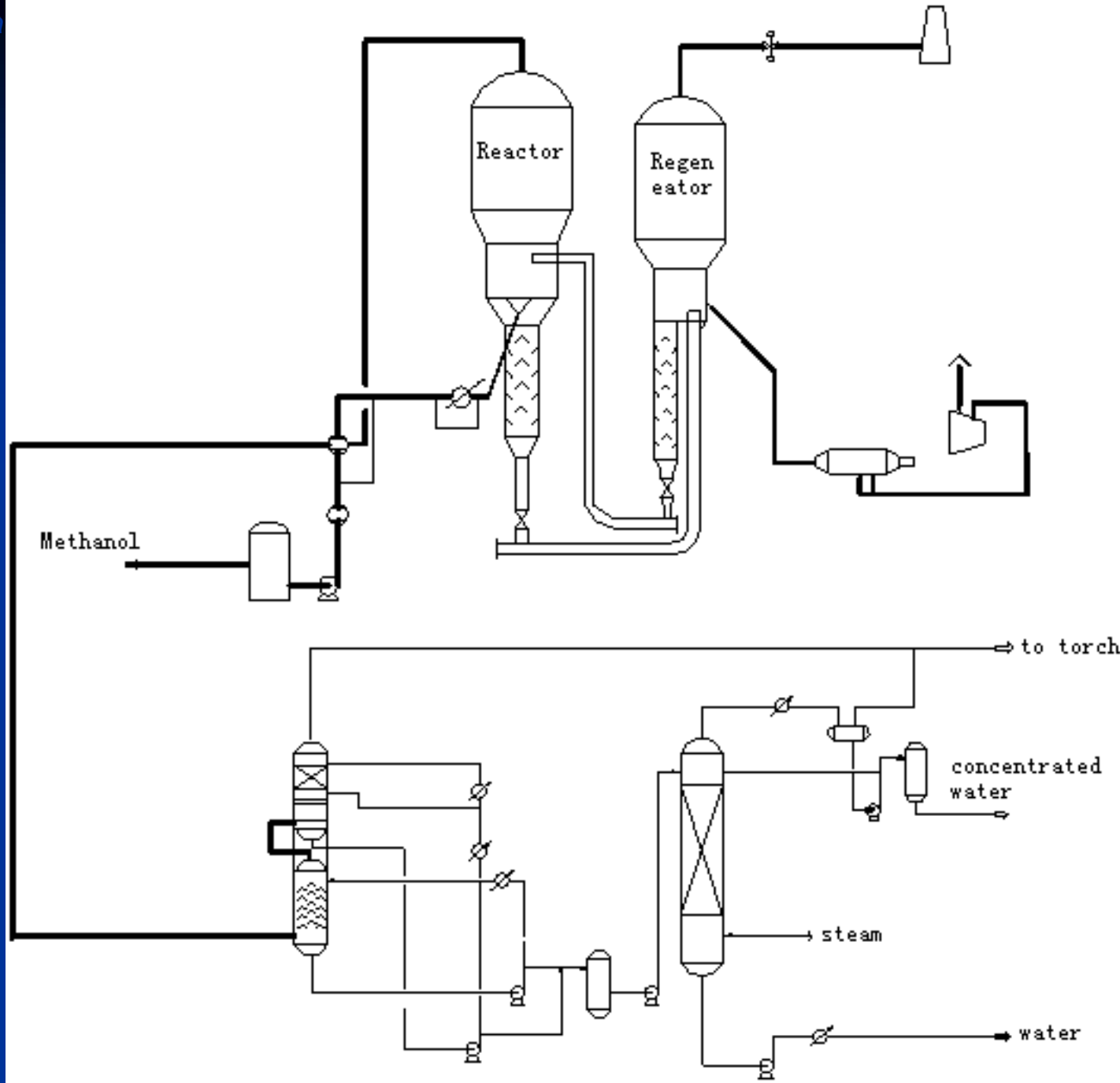
# DMTO Demonstration

- **目标 Objective**
  - 通过工业性试验，开发我国自有知识产权的DMTO 工业化成套技术，为建设以煤为原料生产低碳烯烃的工业化装置奠定技术基础
  - **To develop DMTO technology for the design of large scale commercial units**
- **合作三方 Partner**
  - 中国科学院大连化学物理研究所 **Dalian Institute of Chemical Physics**
    - 提供中试工艺技术和催化剂 **Providing pilot technology for design and the catalyst**
  - 中国石化集团洛阳石油化工工程公司 **Luoyang Petrochemical Engineering Company, Sinopec**
    - 工程放大和试验装置设计 **Engineering design**
  - 陕西新兴煤化工科技发展有限公司 **Shanxi Xinxing Coal Chemical Technology Ltd**
    - 投资建设、管理运行试验装置 **Investment, construction, management, operation**
    - 股东：陕西省投资集团公司，正大煤化有限公司，陕西煤业集团公司 **Joint venture company: Shanxi Investment Group, Zhengda Coal Chemical Ltd, Shanxi Coal and Chemical Group**

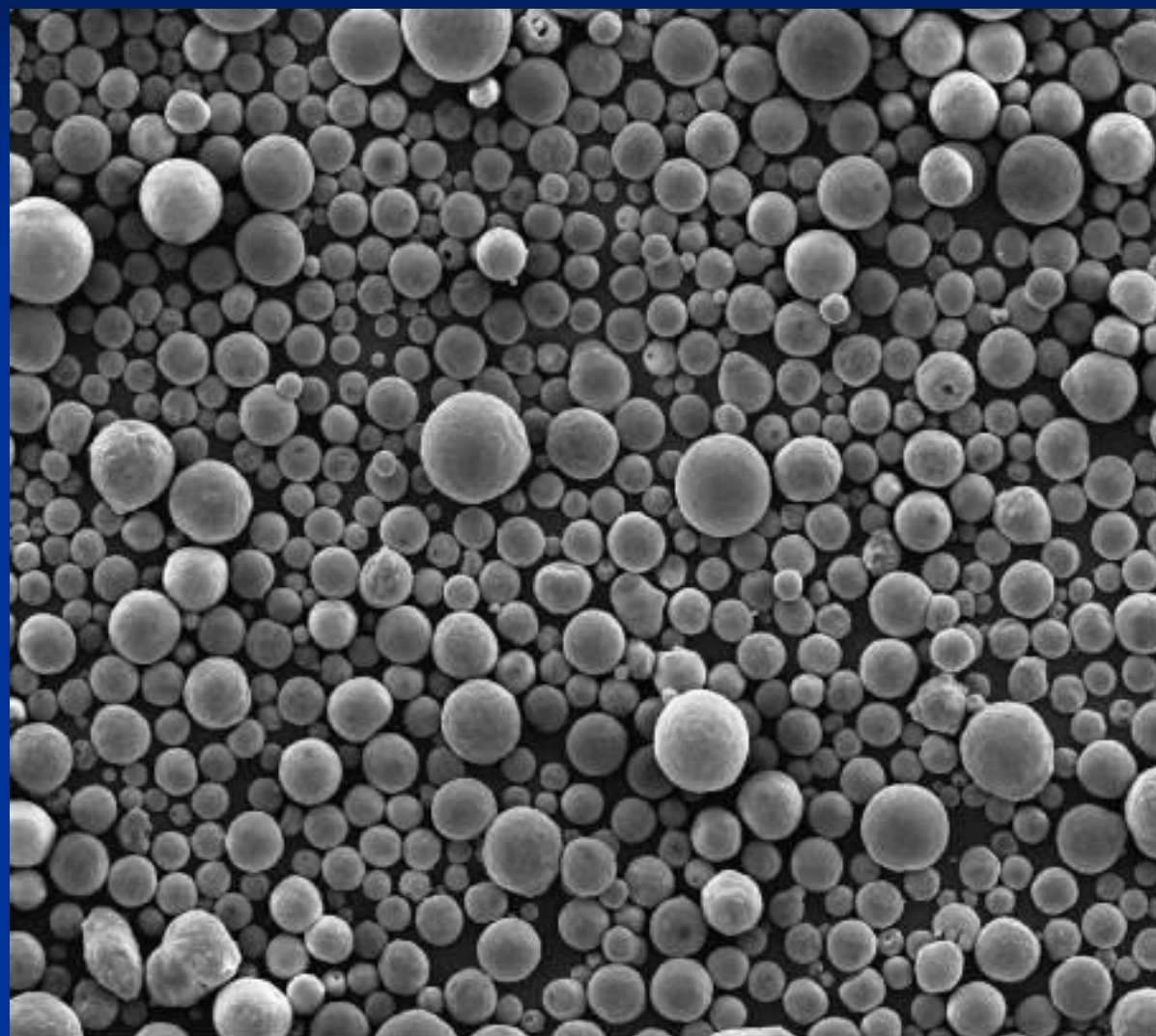
# 工业化试验装置建设及试验 Design and Construction

- 2004年8月项目正式启动 The project started on August 8 of 2004
- 2004年10月11日项目可行性研究报告通过审查 Feasibility study finished and passed on October 11 of 2004
- 2005年2月27日基础设计通过审查 Basic design finished and passed on February 27 of 2005
- 2005年12月份装置建设竣工 Construction finished in December of 2005
- 规模 Scale: 50t/d of MeOH
- 世界第一个同类规模装置 First unit at such scale for MTO demo in the world





# 催化剂 DMTO catalyst



X 100

500  $\mu\text{m}$

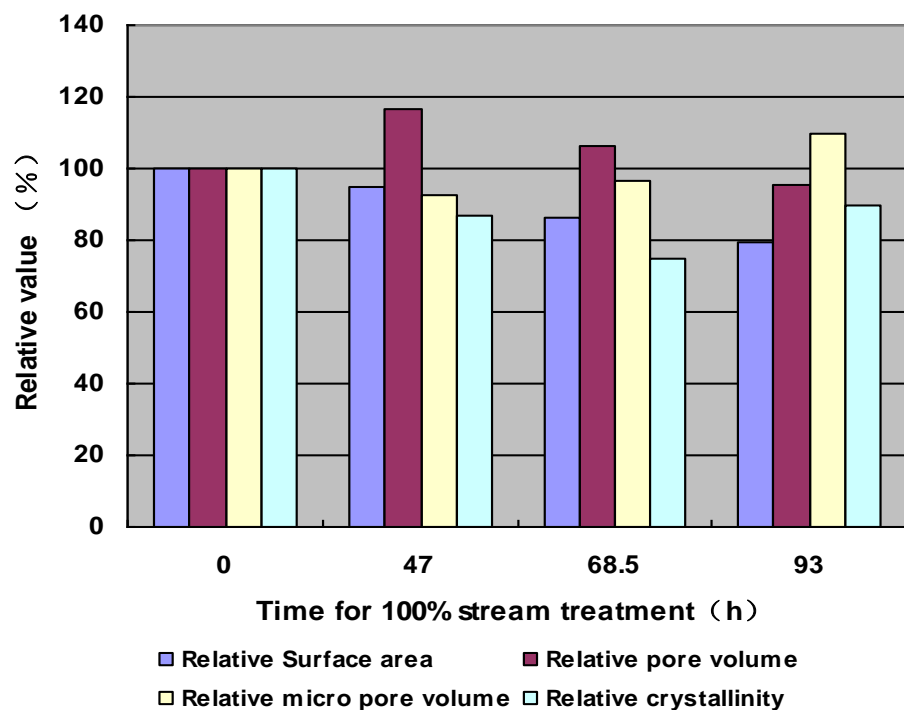
25KV

Chemical Physics, CAS

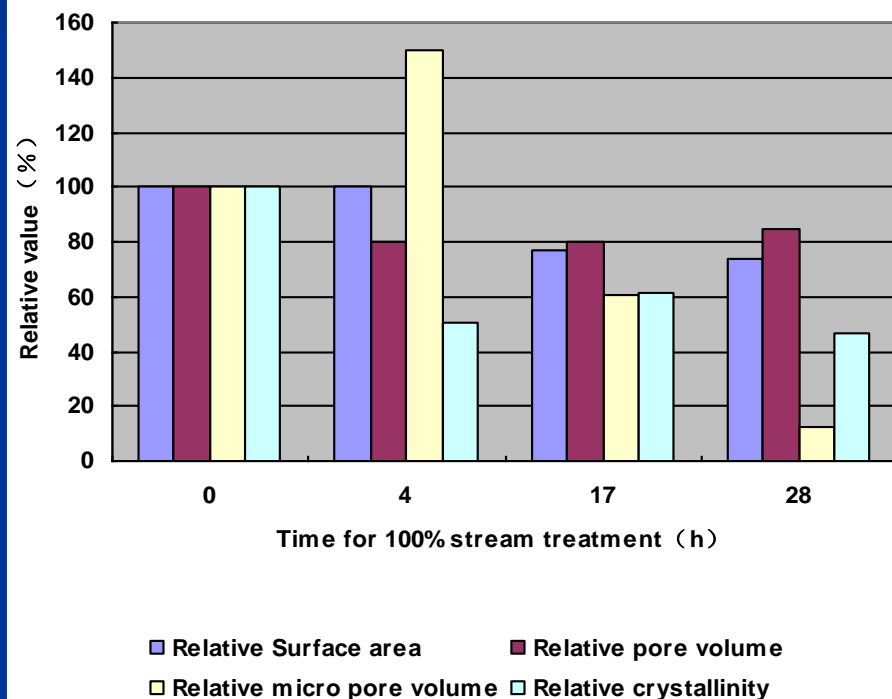
# 催化剂热稳定性和水热稳定性

## Hydrothermal stability of the catalyst

DMTO catalyst

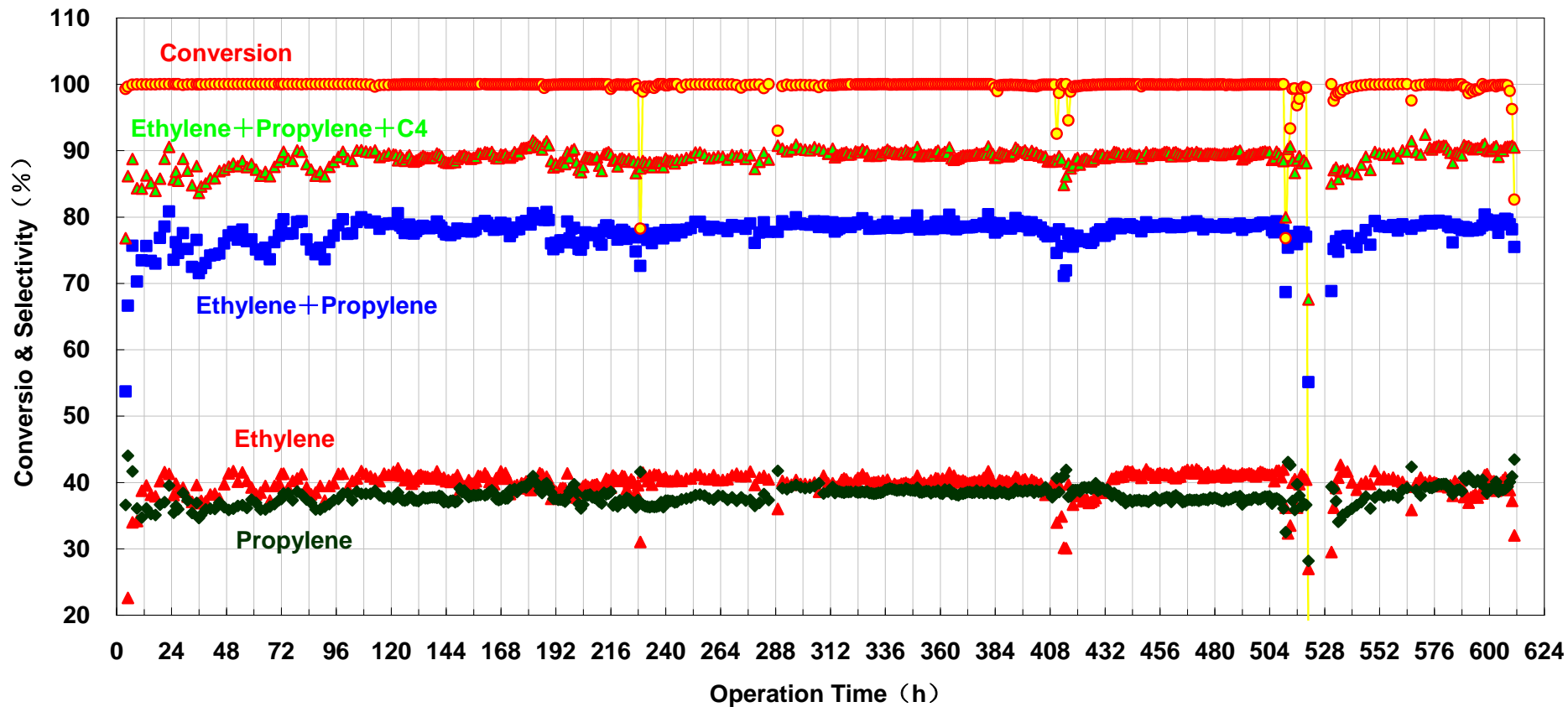


FCC Catalyst

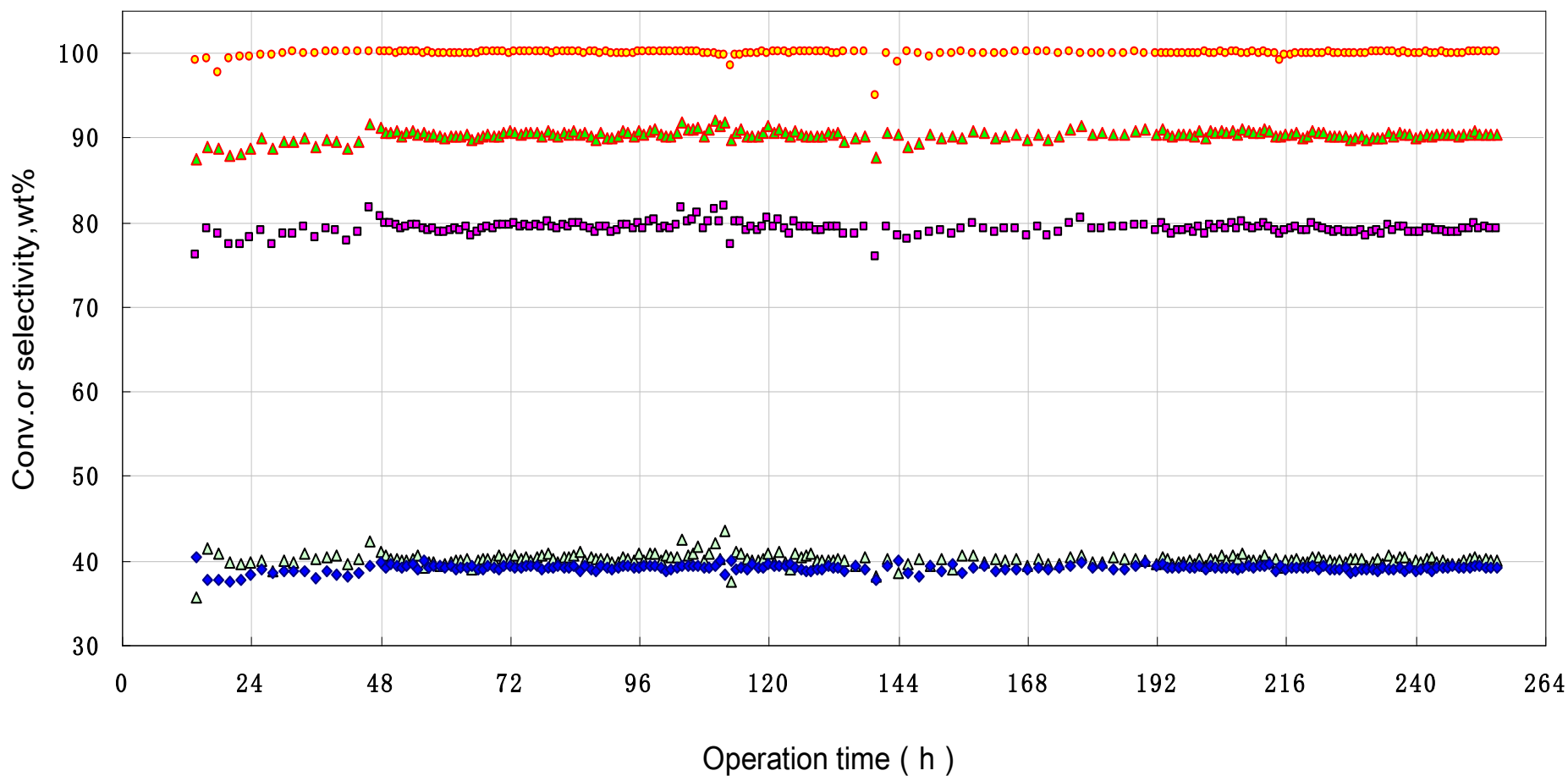


## 条件试验和优化

## Variables test and optimization



# 典型结果 Typical results



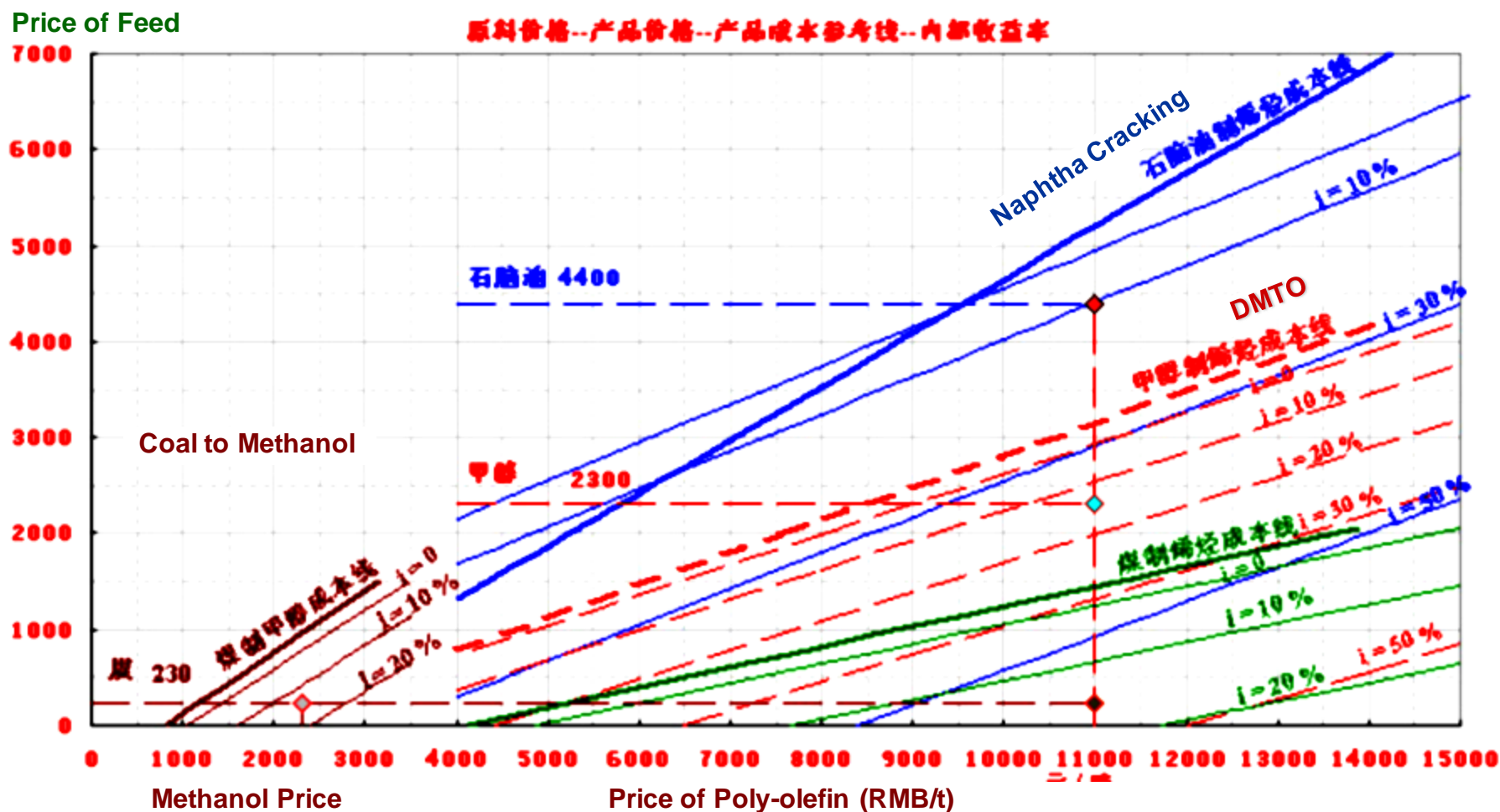
## DMTO工业性试验结果

## Results DMTO Demonstration test

项目	DMTO工业性试验	DMTO demonstration
原料	甲醇	MeOH
规模	50吨/天	50t/d
反应器类型	流化床	Fluidized bed
原料单程转化率	大于99%	>99%
乙烯+丙烯 产率wt%	33.73	
乙烯+丙烯 选择性wt%	79.1	
原料消耗/单位质量烯烃	2.96	
催化剂	D803C-II01	

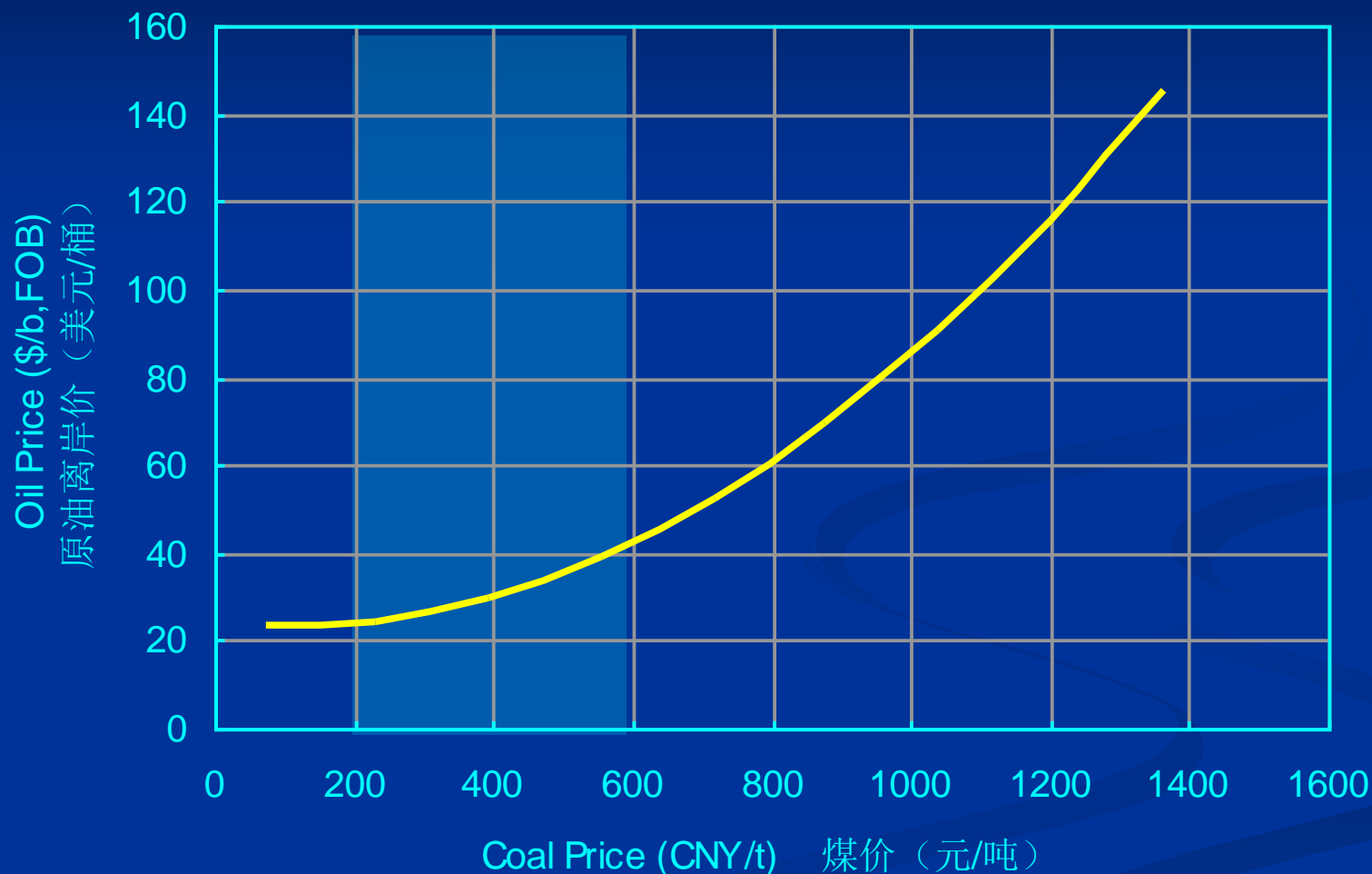
# DMTO和石脑油裂解经济性对比

## Economics: DMTO & naphtha cracking



# 相同烯烃生产成本时煤炭价格与原油离岸价格的对应关系

## Relationship between coal and oil prices at same olefin cost



# DMTO技术工业化应用

## Commercialization of DMTO

- **工业装置建设**                      **Construction of commercial plant**
  - **神华包头项目**                      **Baotou Project of Shenhua Group**
  - **规模**                      **Scale: 600kta olefin**
  - **国家发改委核准 (06.12)** **Approved by NDRC (Dec, 06)**
  - **2010年开车运行**                      **Will be operated in 2010**
  - **世界上第一套煤制烯烃工厂** **First coal to olefin plant in the world**
- **正在向海外技术许可** **The construction of commercially unit will be licensed outside China**
  - **许多国际烯烃公司寻求技术许可或合作**                      **Many international olefin companies have contact us for the technology licensing**
  - **与CBI-Lummus合作**                      **Cooperating with CBI-Lummus**

# 神华包头项目

## Baotou Project of Shenhua Group

Nov 25, 2009



# 甲醇制丙烯

## Methanol to Propylene (MTP)

### ■ FMTP技术

### FMTP Technology

### ■ 合作各方

- **中国化学工程集团公司** China National Chemical Engineering Group Co., Ltd
- **清华大学** Tsinghua University
- **淮南化工集团公司** Anhui Huainan Chemical Group Co., Ltd

# 开发历程

## Developing Progression

- **1999~2007:** 催化剂合成及工艺技术研究

Catalyst synthesis and technologic research

- **2008.12:** 流化催化剂成功放大生产

Successful scale-up production of the catalyst used in a fluidized bed reactor

- **2009.10:** FMTP工业试验成功

Successful FMTP pilot plant test

**世界第一套流化MTP工业性试验装置 First demonstration unit in the world on Fluidized MTP**

# 3万吨甲醇/年 FMTP工业试验装置 30KTA (Methanol) FMTP Demonstration Plant



Continuously running for 470hr

连续运转470小时

Dalian Institute of Chemical Physics, CAS

# 技术指标 Results

甲醇转化率 %	Methanol Conversion %	99.9
丙烯选择性 (C基) %	Propylene Selectivity (Carbon Based) %	67.3
吨甲醇/吨丙烯	t Methanol/t Propylene	3.39

# 结束语

- 中国发展了DMTO技术和FMTP技术，完成了工业性试验  
DMTO and FMTP technologies have been developed,  
and demonstration tests were finished in China
- DMTO技术的工业应用，将使中国首先实现煤制烯烃过程工业化

The application of DMTO technology will leads to a first commercial coal to olefin process in China

# 致谢

## Acknowledgement

- 国家发改委 National Development and Reforming Committee (NDRC)
- 科技部 Ministry of Science and Technology
- 中国科学院 Chinese Academy of Sciences
- 陕西省政府 Government of Shanxi Province
- 石油和化工协会 Oil and Chemical Association
- 所有的合作伙伴 All partners for technology development
- 神华集团 Shenhua Group
- 从事DMTO和FMTP研究的同事们 Colleagues on DMTO and FMTP

# Thanks !